

IN THE SPECIFICATION

Please replace the paragraph beginning on page 2, line 23, with the following rewritten paragraph.

A more complete appreciation of the invention, and many of the attendant advantages thereof, will be readily obtained, as the same becomes better understood by reference to the following detailed description, when considered in connection with the accompanying drawings, wherein:

Figure 1 schematically shows a typical pulse combustion dryer (PCD) plant.

Figure 2 shows the arrangements of gas and liquid nozzles and the air ring.

Figure 3 shows an in-principle sketch of the swirl-inducing element.

Figure 4 to 10 show silicas dried by the PCD method.

Figure 11 shows the determination of the  $w_k$  coefficient.

Figure 12 shows particle size distributions measured using light scattering of the product dried using PCD and ~~that dried in a spray dryer~~ the particle size distribution of the silica suspension before drying.

Please replace the paragraph beginning on page 12, line 27, with the following rewritten paragraph.

As target parameters, only the particle sizes of the produced powder are discussed here. The results in Figure 12 show that the particle size distributions (measured using laser light scattering) of the product (cyclone) dried using the PCD and that of the initial suspension ~~dried in a spray dryer~~ are virtually ~~identical~~ very similar. This means that the PCD product is significantly coarser than the milled final product described in EP 0 901 986.